

Helsinki 25.3.2003

Rec'd PCT/PT 09 JUL 2004
PCT/FI03/00008

ETUOIKEUSTODISTUS
PRIORITY DOCUMENT

REC'D 04 APR 2003

WIPO PCT



Hakija
Applicant

Borealis Technology Oy
Porvoo

Patenttihakemus nro
Patent application no

20020033

Tekemispäivä
Filing date

09.01.2002

Kansainvälinen luokka
International class

B01J

Keksinnön nimitys
Title of invention

"Chamber"
(Säiliö)

PRIORITY DOCUMENT

SUBMITTED OR TRANSMITTED IN
COMPLIANCE WITH RULE 17.1(a) OR (b)

Täten todistetaan, että oheiset asiakirjat ovat tarkkoja jäljennöksiä
Patentti- ja rekisterihallitukselle alkuaan annetuista selityksestä,
patenttivaatimuksista, tiivistelmästä ja piirustuksista.

This is to certify that the annexed documents are true copies of the
description, claims, abstract and drawings originally filed with the
Finnish Patent Office.

Marketta Tehikoski

Marketta Tehikoski
Apulaistarkastaja

Maksu 50 €
Fee 50 EUR

Maksu perustuu kauppa- ja teollisuusministeriön antamaan asetukseen 1027/2001 Patentti- ja rekisterihallituksen maksullisista suoritteista muutoksineen.

The fee is based on the Decree with amendments of the Ministry of Trade and Industry No. 1027/2001 concerning the chargeable services of the National Board of Patents and Registration of Finland.

Osoite: Arkadiankatu 6 A Puhelin: 09 6939 500
P.O.Box 1160 Telephone: + 358 9 6939 500
FIN-00101 Helsinki, FINLAND

Telefax: 09 6939 5328
Telefax: + 358 9 6939 5328

BEST AVAILABLE COPY

CHAMBER

Field of the invention

5 The invention relates to the preparation of solid catalyst carriers by crystallization, and concerns crystallization chambers, methods for the crystallization of the carrier, and methods for removing the carrier from the crystallization chamber.

Background of the invention

10 Polymerization catalysts, such as Ziegler-Natta type catalysts, are usually deposited on solid carrier particles. The chemical composition, the structure of the surface, the morphology, and the size of the particles are important for the activity of the catalyst and for the properties of the polymer to be produced.

15 Certain carriers, such as $MgCl_2 \cdot (ROH)_n$, in which R is an alkyl group and n is 1 to 6, are prepared by melting the substance and then crystallizing the melt in a spraying chamber. The crystallized particles are screened in order to remove too small and too big particles. The melt may be sprayed e.g. through a rotating nozzle, as described in EP 655 073. One problem in such processes is that the carrier tends to stick and agglomerate on the walls of the chamber. This decreases the yield and quality of the carrier. Pneumatic hammers have been used for removing the carrier from the walls. This has, however, not been very effective. Hammering also easily damages the chamber.

Summary of the invention

25 Now a chamber for the preparation catalyst carrier by crystallization, a method for preparing such carrier in a chamber, and a method for removing such carrier from a chamber have been invented in accordance with the independent claims. Some preferable embodiments of the invention are described in the dependent claims.

30 In accordance with the invention, the chamber is provided with an acoustic generator, which produces a strong sound which loosens the material from the walls of the chamber. The intensity of the sound may be e.g. 100 to 150 dB, preferably 120 to 140 dB, and most preferably 130 to 135 dB. The frequency of the sound may be e.g. 100 to 1000 Hz, preferably 400 to 600 Hz. The duration of the sound signal used may be e.g. 1 to 10 seconds, such as 3 to 7 seconds. The generator is preferably

used at suitable intervals, e.g. at intervals of 0.2 to 2 minutes, preferably 0.3 to 0.7 minutes.

5 The acoustic generator may such as to comprise a vibrating metal diaphragm which is vibrated pneumatically. The generator if usually provided with a horn. The horn should be pointed downwards in the chamber.

The chamber is usually a closed vessel surrounded by walls. The generator is preferably mounted in the top wall of the chamber.

10 The material is preferably removed from the chamber from its bottom. The chamber is typically an upright cylindrical chamber with a conical bottom. The volume of the chamber is typically 10 to 30 m³, such as 15 to 20 m³.

The carrier may be e.g. a magnesium containing carrier, such as $\text{MgCl}_2 \cdot (\text{ROH})_n$, in which R is an alkyl group and n is 1 to 6. Such a carrier is used especially for Ziegler-Natta type olefin polymerization catalysts. Silica is another typical carrier material.

15 In the crystallization chamber, melted material is sprayed into the chamber where it is cooled and crystallized. Cooling gas may be blown into the chamber. The cooling gas is preferably an inert gas, such as nitrogen. According to one embodiment, the melt is fed through a nozzle on the top of the chamber. Cooling gas is also fed on the top of the chamber. Additional cooling gas may be fed on a lower position. The
20 second cooling gas usually has lower temperature.

In accordance with the invention, sticking of the catalyst material on the walls and outlet of the chamber and agglomeration of the catalyst material particles is effectively prevented. This is especially advantageous when the material is removed continuously from the chamber. The fraction of too large particles to be rejected is also
25 thus decreased. The quality of the material is not decreased. No damage is caused to the chamber.

Brief description of the drawings

The enclosed drawings form a part of the written description of the invention.

Fig. 1 shows the preparation of a catalyst carrier by a spraying process.

Detailed disclosure of some embodiments of the invention

Fig. 1 describes the preparation of a $\text{MgCl}_2 \cdot (\text{C}_2\text{H}_5\text{OH})_n$ carrier material. The material is melted and fed through line 1 and nozzle 2 on the top of spraying chamber 3. The flow rate of the melt is F1 and temperature T1. Nitrogen is fed through line 4 on the top of the chamber. The flow rate is F2 and the temperature T2. T2 is lower than T1. A second nitrogen flow is fed through line 5 into the lower part of the chamber just above the conical bottom. The flow rate is F3 and the temperature T3. T3 is lower than T2. The carrier material crystallizes in the chamber and falls at the bottom, from where it is continuously removed through line 6 to screen 7. Gases are removed from the chamber through line 8.

An acoustic generator 9 (Nirafon, Lahti, Finland) is mounted inside the chamber 3 at the top, the horn pointing downwards into the chamber. The generator comprises a vibrating diaphragm at the frequency of 500 Hz. The maximum intensity of the sound is 135 dB. The horn is operated with 7 to 8 bar nitrogen.

The process was run under the following conditions:

F1	T1	F2	T2	F3	T3
kg/h	°C	kg/h	°C	kg/h	°C
25	115	340	64	650	-21

The acoustic generator 8 was blown for 5 sec after each 30 sec.

The process could be run without the material blocking the bottom outlet or sheeting the chamber walls. The longest uninterrupted run was 15 days. Even after that no sign of the carrier depositing on the walls or outlet was found.

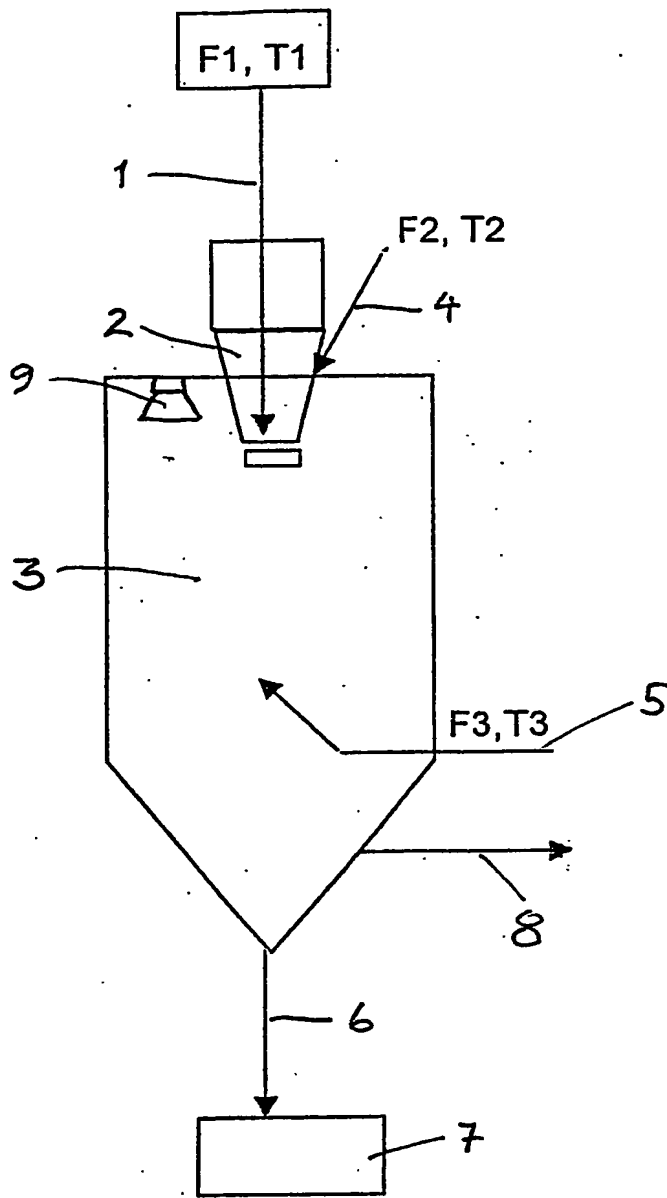
As a comparison, the acoustic generator 8 was switched off. An immediate small drop in the outlet rate was observed. After 6 hours the outlet was totally blocked and it had to be opened. The run was continued and after hours the outlet was almost totally blocked again. When the acoustic generator was taken in use again, after 15 hours a sudden flood of material was observed. This material had obviously been deposited on the walls of the chamber and was now suddenly dropped.

Claims

1. Chamber for the crystallization of solid catalyst carrier, characterized in that the chamber is provided with an acoustic generator (9).
2. Chamber according to claim 1, wherein the chamber comprises a top wall and the acoustic generator (9) is mounted in the top wall.
3. Method for the preparation of solid catalyst carrier, in which method the carrier is formed in a chamber, characterized in that the inside of the chamber is subjected to a sound generated by an acoustic generator (9).
4. Method according to claim 3, wherein the intensity of the sound is at least 100 dB, preferably at least 120 dB, and most preferably at least 130 dB.
5. Method according to claim 3 or 4, wherein the frequency of the sound is 100 to 1000 Hz, preferably 400 to 600 Hz.
6. Method according to any of claims 3 to 5, wherein the duration of the sound is 1 to 10 seconds, preferably 3 to 7 seconds.
7. Method according to any of claims 3 to 6, wherein the sound is generated periodically, such as at intervals of 0.2 to 2 minutes, preferably at intervals 0.3 to 0.7 minutes.
8. Method for removing crystallized solid catalyst carrier from a chamber, characterized in that the inside of the chamber is subjected to a sound generated by an acoustic generator (9) for loosening the carrier from the chamber.
9. Method according to claim 8, wherein the carrier is removed continuously from the chamber.
10. Use of an acoustic generator for loosening crystallized solid catalyst carrier from a chamber.

(57) Abstract

The invention relates to a chamber for the crystallization of solid catalyst carrier. The chamber is provided with an acoustic generator (9) for loosening the carrier from the walls of the chamber.



BEST AVAILABLE COPY